

TABLE I. Properties of nitrogen along the melting curve.

$P_m$ (kg/cm <sup>2</sup> )	$T_m$ (°K)	$\Delta V_m$ (mm <sup>3</sup> /g)	$n^a$	av dev. <sup>b</sup> (±%)	$V_l$ (cm <sup>3</sup> /g)	$\alpha_l$ (10 <sup>3</sup> deg <sup>-1</sup> )	$\alpha_s$ (10 <sup>3</sup> deg <sup>-1</sup> )
1	63.14	(90.13) <sup>c</sup>					
79.0	64.84	84.65	4	0.42	1.1495	4.56	4.40
202.0	67.40	77.71	3	0.55	1.1376	4.14	4.03
354.7	70.46	72.69	4	0.37	1.1229	3.49	3.41
504.1	73.36	66.90	3	0.16	1.1081	3.17	3.12
710.9	77.24	62.34	6	0.58	1.0984	2.92	2.88
1066.8	83.57	55.91	4	0.16	1.0771	2.39	2.37
1422.7	89.54	51.24	6	0.27	1.0582	2.03	2.02
1920.7	97.40	44.50	4	0.26	1.0334	1.68	1.68
2631.9	107.83	39.71	4	0.31	1.0081	1.07	1.08
3555.6 (18503) <sup>c</sup>	120.29 (256.4) <sup>c</sup>	33.52 0	5	0.93	0.9782	0.94	0.95

<sup>a</sup>  $n$  = number of  $\Delta V_m$  determinations at each  $P_m$ .

<sup>b</sup> The average deviation from the mean of the  $n\Delta V_m$  determinations.

<sup>c</sup> Values in parentheses are extrapolations of the measurements.

#### IV. DISCUSSION

##### A. Comparison with Previous Results

The only previous measurements of  $\Delta V_m$  for  $N_2$  were made by Bridgman<sup>2</sup> over the pressure range 1000–6000 kg/cm<sup>2</sup>. His piston displacement method is considered less reliable than the present method in that his low-temperature fluid density was obtained indirectly by using high-pressure  $P$ - $V$ - $T$  relations for gas at room temperature. Furthermore, his temperature scale is in doubt, for he apparently used, as calibrating baths, liquid  $N_2$  and  $O_2$  of unspecified purity. Probably the most troublesome part of any method is in filling the cell completely with solid. Bridgman recognized this and sought to fill his cell completely by raising and lowering the bath around the cell. Even so, he concluded that his higher  $\Delta V_m$  values were more reliable. In the present observations, it was found that the most reproducible data resulted from raising the freezing bath at a slow, uniform rate. A comparison of the present results with Bridgman's in Fig. 2 indicated fair agreement in general, although he reports several values that appear to be 25% too small. Also on the graph is the value of  $\Delta V_m$  at 1 atmos calculated from the initial slope of the melting curve<sup>1</sup> and the  $\Delta H_m$  of Giauque and Clayton<sup>17</sup>; it agrees to 0.7% with an extrapolation of the present measurements.

Figure 3 shows the present  $V_l$  data compared with: those extrapolated from Benedict's<sup>14</sup> measurements (made at temperatures from 5 to 20° higher than  $T_m$ ); the value at the triple point extrapolated from the measurements of Mathias *et al.*<sup>18</sup> along the vapor pressure curve; and Bridgman's<sup>2</sup> measurements. The Benedict results<sup>14</sup> covered a wide range of pressure and temperature and were put into two equations of state, Eq. (8) of Paper I and Eq. (2) of Paper II. Since the latter resulted from a more restricted range, it should not be expected to extrapolate as well to the melting

<sup>17</sup> W. F. Giauque and J. O. Clayton, *J. Am. Chem. Soc.* **55**, 4875 (1933).

<sup>18</sup> Mathias, Onnes, and Crommelin, *Leiden Comm. No. 145c* (1914).

curve. However, his Eq. (I-8) along with the Mathias value fit the present data within 0.2%, while Bridgman's values differ by as much as 6%.

The only comparative data on  $\alpha_l$  result from differentiation of Benedict's equations of state and are given in Fig. 4. If one considers the extrapolation of his results and the accuracy of the present measurements, the agreement is adequate.

##### B. Formulas for Specific Volume and Thermal Expansion

A comparison of the constants of Eq. (2) with those of Eq. (3) indicates that the following relations should hold for  $V_s$  and possibly for  $V_l$ :

$$a' = a (= 1638),$$

$$b' = \frac{RT_0}{2a^{1/c}} \left( \frac{1+2c}{c-1} \right) (= 8.94),$$

$$c' = \frac{1}{c} - 1 (= -0.44),$$

where  $R$  is the gas constant,  $T_0$  is the triple point temperature, and the numbers in parentheses are obtained from  $a$ ,  $b$ , and  $c$ , the constants in the Simon melting equation for  $N_2$  as measured previously.<sup>1</sup> It is readily apparent from Table II that there is some consistency in the relationships for  $a'$  of  $V_l$ ,  $\alpha_l$ , and  $\alpha_s$ ;  $b'$  of  $V_l$  and  $V_s$ ; and  $c'$  of  $V_l$  and  $V_s$ . It is rather surprising that the  $a'$  for  $V_s$ , which should come closest to  $a$ , deviates the most.

##### C. Thermodynamic Properties of Melting

From the Clapeyron equation and Eqs. (1) and (3), one can obtain the following expressions for the thermal properties of melting,

$$\Delta H_m = c(P-a)[A - B \log_{10}(P+C)], \quad (4)$$

and

$$\Delta S_m = cb^{1/c}(P-a)^{(c-1)/c}[A - B \log_{10}(P+C)], \quad (5)$$

where, for  $N_2$ ,

$$\begin{aligned} a &= -1638.3 \text{ kg/cm}^2, & A &= 0.20707 \text{ cm}^3/\text{g}, \\ b &= 0.97678 \text{ kg/cm}^2/\text{deg}, & B &= 0.048457 \text{ cm}^3/\text{g}, \\ c &= 1.7910, & C &= 257.98 \text{ kg/cm}^2. \end{aligned}$$

Up to 3500 kg/cm<sup>2</sup>, the error in computed values of  $\Delta H_m$  and  $\Delta S_m$  should be <1%. At  $P=1$  atmos, Eq. (4)

TABLE II. Constants in Eq. (2) for specific volumes and thermal expansion coefficients.

	$a^*$ (kg/cm <sup>2</sup> )	$b^*$ (cm <sup>3</sup> /g or deg <sup>-1</sup> )	$c^*$
$V_l$	1695.3	3.4402	-0.14671
$V_s$	4486.5	5.8963	-0.20386
$\alpha_l$	1904.0	754.1	-1.5851
$\alpha_s$	2035.8	950.6	-1.6063